

Review: Compact Helical Counter-Flow Heat Exchanger Numerical Analysis

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ABSTRACT: The execution of compact counter stream warm exchangers with helically formed sections is inspected employing a 1-D explanatory show and compared with a high-fidelity 3-D numerical reenactment. The 1-D show is able of evaluating the common patterns related with the warm exchange execution and liquid weight misfortunes, though the tall constancy 3-D numerical model is required to supply more

I. INTRODUCTION

Because of its compact construction and excellent heat transfer coefficient, heat exchangers are widely used in commercial applications such as power generation, nuclear industry, system vegetation, heat recuperation systems, refrigeration, food industry, and so on. Due to their ease of manufacture, helical coils with circular move phases were widely employed in a variety of package styles. Because of the existence of centrifugal forces, floating in a curved tube differs from floating in a straight tube. These centrifugal forces form a secondary flow parallel to the primary direction of flow, with circulatory results that raise both the friction factor and the fee of heat switch. The amount of secondary drift advanced within the tube is proportional to the tube diameter (d) and coil diameter (D). Because of the more desirable warmth switch in shell and helical coiled configurations, the investigation of flow and warmth switch characteristics in the curved tube is critical. Creating fluid-to-fluid helical warmth exchangers (fluid is available on both sides of the tube wall) necessitates a thorough understanding of the warmth switch mechanism on both sides of the tube wall. Despite extensive research on the warmth transmission coefficients within coiled tubes, little work has been documented on the outside warmth transfer coefficients. One of the severe problems is warmth switch fluid, which disrupts the scale and value of warmth exchanger structures. Traditional fluids such as oil and water have partial heat switch potential. It is our first priority to produce unique types of fluids in order

precision. Warm exchange rate and weight drop on straight and helical blades warm exchangers were compared by keeping the length of the blade and the water powered breadth of the channel consistent

Key Word: Helical Fin Heat Exchanger, Counter Flow, Thermal Conductivity, Hot fluid, Cold fluid, Fins, Annular Fin Heat Exchanger.

to reduce fees and fulfil the growing demand of industry and commerce. Through threat, advances in nanotechnology make it possible to achieve improved performance and cost savings in heat transmission technologies. Nanoparticles are occupied as the dazzling establishment of materials with potential applications in the warmth transfer place.

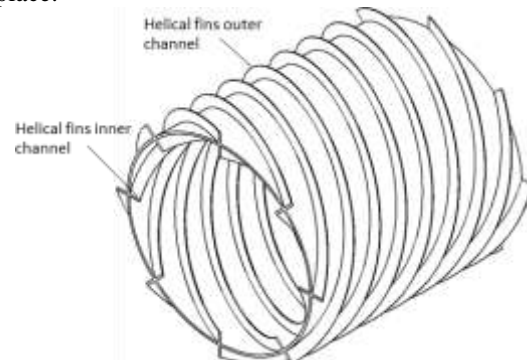


Figure 1 Helical Fin Heat Exchanger

Heat exchanger execution can be progressed by choosing higher warm conductivity working liquids or increment the warm exchanger surface range or modifying the introduction of the channel and changing the geometry. In his think about the warm exchanger execution was made strides by expanding the warm exchange surface region by spiral blades.

To extend the warm exchanger execution straight outspread blades were included between the mid pipe and external pipe as well as deepest pipe.

II. LITERATURE REVIEW

Yinhai Zhu et.al [1] The heat transfer behaviors in developed and developing region on four basic fins of plate fin heat exchanger was numerically analyzed by Yinhai Zhu and Yanzhong Li. Three dimensional geometries such as plain fin, strip offset fin and wavy fin were investigated for the Reynolds number range of 132.3 to 1323. Data reduction method was used to calculate the local Nusselt number and pressure drop. Heat transfer characteristics were obtained using j and f factors.

Lingadi Tang et al [2] Flow characteristics inside the helical pipe was analyzed by Lingadi Tang. In this study, the numerical simulation was carried out to find velocity distribution, pressure field and secondary flow variation by varying coil parameters. It also stated that secondary flow is the major factor in pressure loss, however, increase in curvature radius and coil pitch can reduce friction factor. The numerical method was validated by experimental analysis and found that the deviation between the numerical and experimental analysis was 2.9%.

Vinous M. Hameed et al. [3] The characteristic of flow inside the helical coil, pressure drop, and heat transfer have been studied by many investigators. The performance of triangular finned tube heat exchanger was performed experimentally and numerically investigated by Vinous M. Hameed. Experimental work carried out by designing and manufacturing of triangular fins using copper material and the results showed that the enhancement of heat dissipation for triangular finned tube is 3 to 4 times than smooth tube. Numerical simulation was carried out using COMSOL CFD package model and reported that the numerical results showed good agreement with experimental work.

Pranita Bichkar et.al. [4] doing research on the impact of various types on Shell and Tube Heat Exchangers. This research offers numerical simulations of unsegmented, double segmented, and vertical arrangements. This implies that the shell has an influence on the pressure drop of the shell and tube heat exchanger. Unsegmented blocks exhibit the creation of dead zones in which the heat transfer cannot be turned on. When compared to single segment beams, double section beams lessen vibration damage. Because dead zones are eliminated when using a vertical shell, pressure is reduced. Fewer dead zones result in a greater heat transfer. Reduced stress results in less pump energy, which boosts

system efficiency. The comparison results reveal that the vertical is more beneficial than the horizontal.

Vidula Vishnu Suryawanshi et.al. [5] carried out research on the designing and assessment of helical coil heat exchangers. CFD analyses are performed in this work on several compounds with varying sizes. The following tasks must be completed to further develop the helical heat exchanger: wall temperature and consistent wall heat flux in both laminar and turbulent flow. To maximize the heat transfer coefficient, examine the results and alter the spiral winding pitch.

The Mohamed Ali et.al. [6] The experimental inquiry of natural convection created to examine, constant type natural convection became obtained from turbulent natural convection to water. The experiments were carried out with a coil diameter to tube diameter ratio of four for five and ten coil tubes, as well as a pitch to outer diameter ratio of five. He correlated Rayleigh number for two distinct coil sets and discovered that the heat transfer coefficient falls with coil length for tube diameter $d_o = 0.012$ m but increases with coil length for $d_o = 0.008$ m. For a maximum heat transfer coefficient, a tube diameter of 0.012 m with either five or ten coil turns yields a significant D/d_o .

III. PROBLEM FORMULATION

Experimental analysis on a 3D printed helical heat exchanger was complicated by size limitations. In addition, the experimental work is mainly focused on measuring pressure and temperature at the outlet and inlet of the heat exchanger, while the 3D numerical simulation allows a clear understanding of the flow phenomenon inside the helix. screws as well as calculate the heat exchanger's efficiency.

IV CONCLUSION

This work determined the flow characteristics in the spiral segment using 3D computer analysis. The numerical results of four different cases with mass flows of 0.01 kg/s and 1 kg/s of hot and cold liquid mass flows, respectively, were calculated and compared with the model. one-way analysis. The finite volume method is used to solve the conservation of mass, momentum and energy equations. The K- ω SST model was taken into account to model turbulence in a helical heat exchanger. Analytical modeling can be used as a tool to quickly define and optimize new heat exchanger designs with a

now defined level of accuracy (compared to a detailed 3D CFD model).)

Maximum outlet temperature and pressure drop difference between 3-D CFD 1-D analysis results have been determined for several HEX concepts

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